

Instructions:

- 1) Question No 1 is compulsory
- 2) Answer any 3 from the remaining.
- 3) Assume suitable data if necessary.

- Q-1 Answer any 4 questions. 20
- a) A rectangular slab ($k = 10 \text{ W/m-K}$) of thickness 15 cm and inside temperature of 400°C is insulated by a materials of thickness 10 cm ($K = 30\text{W/m-K}$). The ambient air is at 28°C and the outside convective heat transfer coefficient is $15 \text{ W/m}^2\text{K}$. Determine the steady state heat transfer per unit surface area and the temperature of outside surface of the slab and the insulation.
 - b) In an oil cooler, oil ($m=2500\text{kg/hr}$ and $C_p = 1.9 \text{ kJ/kg-K}$) at 160°C is cooled by water ($m=1500 \text{ kg/hr}$ and $C_p = 4.187 \text{ kJ/kg-K}$) entering at 35°C . Determine Capacity ratio, NTU and effectiveness if the overall heat transfer coefficient is $300 \text{ W/m}^2\text{K}$. Assume parallel flow.
 - c) A pipe, 2cm diameter, at 40°C is placed in (i) an air flow at 50°C with $h = 20\text{W/m}^2\text{K}$ OR in (ii) water at 30°C with $h = 70\text{W/m}^2\text{K}$. Find the heat transfer per unit length of the pipe and comment on the results in both cases.
 - d) Define Fin efficiency and Fin effectiveness. Explain in brief factors affecting fin effectiveness.
 - e) What is the mode of heat transfer in Vacuum? Define absorptivity, reflectivity and transmissivity.
- Q-2 a) Water (mass = 1.4 kg/s , $C_p = 4.187\text{kJ/kg-K}$) is heated from 40°C to 70°C by an oil (mass = 2 kg/sec , $C_p = 1.9 \text{ KJ/kg-K}$) entering at 110°C in a counter flow heat exchanger. If overall heat transfer coefficient is $350 \text{ W/m}^2\text{K}$, calculate the surface area required. 10
- b) Derive the temperature profile equation for a cylindrical system from the general differential equation stating the assumptions for one dimensional steady state heat transfer. 10
- Q-3 a) A steel pipe of OD 0.15m lies 2m vertically and 8m horizontally in a large room with an ambient temperature of 30°C . The pipe surface is at 250°C and has an emissivity of 0.6. Estimate the total heat loss (due to convection and radiation) from the pipe to the atmosphere. Properties at film temperature : $\nu = 27.8 \times 10^{-6} \text{ m}^2/\text{s}$, $k = 0.035 \text{ W/mK}$, $Pr = 0.684$.
[Take $Nu = 0.13 (Gr.Pr)^{1/3}$ if the flow is turbulent OR $Nu = 0.53 (Gr.Pr)^{1/4}$ if the flow is Laminar.] 10
- b) What is lumped system analysis? When is it applicable? 4
 - c) Draw a neat boiling curve for water and mark the different regions. 6
- Q-4 a) A furnace door, 1.5 m high and 1m wide is insulated from inside and has an outer surface temperature of 70°C . If the surrounding ambient air is at 30°C calculate steady state heat loss from the door. Take the properties from at film temperature 50°C are $\rho = 1.093\text{Kg.m}^3$, $\nu = 17.95 \times 10^{-6} \text{ m}^2/\text{s}$, $Pr = 0.698$ $C_p = 1.005\text{J/kg-K}$, use the correlation $Nu = 0.13 (Ra)^{1/3}$ 10
- b) A longitudinal copper fin ($k=380\text{W/m-K}$) 600 mm long and 5 mm diameter 6

TURN OVER